

IN THE CLAIMS

Please amend the claims as follows:

Claim 1. (currently amended) A process for producing closed-celled rigid polyurethane foams by reacting

- a) crude MDI having an NCO content of from 29 to 33% by weight and a viscosity at 25°C in the range from 150 to 1000 mPa•s with
- b) compounds having at least two hydrogen atoms reactive toward isocyanate groups, in the presence of
- c) catalysts, and
- d) blowing agents,

which comprises the presence, among the compounds having at least two hydrogen atoms reactive toward isocyanate groups, of at least one graft polyol, wherein said closed-celled rigid polyurethane has a proportion of closed cells in the foam of at least 88%

wherein said graft polyol is prepared by in-situ polymerization of ethylenically unsaturated monomers in polyether alcohols having a functionality of from 2 to 8 and having a hydroxy value in the range from 100 to 800 mg KOH/g, obtained by an addition reaction of alkylene oxides onto H-functional starter substances, the starter substances having been selected from the group consisting of polyfunctional alcohols, sugar alcohols, aliphatic amines, and aromatic amines.

Claim 2. (previously presented) A process as claimed in claim 1, wherein the amount used of the graft polyol is up to 100% by weight, based on component b.

Claim 3. (previously presented) A process as claimed in claim 1, wherein the amount used of the graft polyol is from 0.5 to 70% by weight, based in each case on component b.

Claim 4. (previously presented) A process as claimed in claim 1, wherein the amount used of the graft polyol during the production of rigid polyurethane foams for use in refrigeration equipment is from 3 to 70% by weight, based on component b.

Claim 5. (previously presented) A process as claimed in claim 1, wherein the amount used of the graft polyol during the production of rigid polyurethane foams for use in sandwich components is from 0.5 to 35% by weight, based on component b.

Claim 6. (previously presented) A process as claimed in claim 1, wherein the graft polyol has a hydroxy value in the range from 20 to 210 mg KOH/g.

Claim 7. (original) A process as claimed in claim 1, wherein the graft polyol particle distribution has a maximum at from 0.1 to 8  $\mu\text{m}$ .

Claim 8. (previously presented) A process as claimed in claim 1, wherein the graft polyol has a bimodal particle size distribution.

Claim 9. (canceled)

Claim 10. (previously presented) A process as claimed in claim 1 wherein the graft polyol is prepared by in-situ polymerization of ethylenically unsaturated monomers in polyether alcohols which are obtained by an addition reaction of alkylene oxides onto tolylenediamine, using basic catalysis.

Claim 11. (previously presented) A process as claimed in claim 1, wherein the graft polyol is prepared by in-situ polymerization of ethylenically unsaturated monomers in polyether alcohols which are obtained by an addition reaction of alkylene oxides onto trimethylolpropane, using basic catalysis or catalysis by multimetal cyanide complexes.

Claim 12. (previously presented) A rigid polyurethane foam produced by the process of claim 1.

Claims 13-16 (canceled)

Claim 17. (previously presented) The process of claim 1, wherein said closed-celled rigid polyurethane has a proportion of closed cells in the foam of at least 95%.

Claim 18. (previously presented) The process of claim 1, wherein said graft polyol is prepared via in-situ polymerization of ethylenically unsaturated monomers in polyether alcohol.

Claim 19. (previously presented) The graft polyol of claim 13, wherein said graft polyol is prepared via in-situ polymerization of ethylenically unsaturated monomers in polyether alcohol.